

Thermochimica Acta 255 (1995) 329-340

thermochimica acta

# On-line method for isothermal kinetic analysis

H.P. Nawada\*, O.M. Sreedharan

Thermodynamics Section, Metallurgy Division, IGCAR, Kalpakkam, Tamil Nadu-603 102, India

Received 16 June 1994; accepted 1 October 1994

# Abstract

The kinetic analysis of any isothermal process is based on compliance with the equational form  $g(\alpha) = kt$ , which requires an a priori knowledge of the final property change  $\Delta p_{\infty}$ . It is therefore imperative that this equation is not applied to incomplete reactions. A new on-line method has therefore been developed here which gives analytical solutions to well known mechanisms of reaction without recourse to  $\Delta p_{\infty}$ . In some cases, where  $\Delta p_{\infty}k$  appears as a product or exponential terms are to be found, computer based numerical methods have been adopted to solve the equations. The deciphering of the mechanism and the evaluation of k without waiting for the completion of a TG run has been demonstrated with a hypothetical TG curve.

Keywords: Accelerating rate equation; Decelerating rate equation; Kinetic analysis; On-line method; Sigmoid rate equation

# 1. Introduction

After reviewing current methods of evaluating the rate constant k and pointing out some of the inherent weaknesses of the non-isothermal method [1], a technique is outlined for the determination of k during the course of an actual isothermal experiment. In isothermal kinetic studies involving at least one solid phase, the rate constant is usually represented by an equational form

$$g(\alpha) = kt \tag{1}$$

\* Corresponding author.

0040-6031/95/\$09.50 © 1995 – Elsevier Science B.V. All rights reserved SSDI 0040-6031(94)02139-2

Rate mechanisms		g(x) = f(kt) functional form	$\alpha = f(kt)$ functional form
<ol> <li>Accelerating rate equations         Power law         Exponential law     </li> </ol>	E1 P1	$\alpha^{1/n} = kt$ ln $\alpha = kt$	$\begin{aligned} \alpha &= (kt)^n \\ \alpha &= \exp(kt) \end{aligned}$
<ol> <li>Sigmoid rate equations (nucleation Avrami-Erofeev Avrami-Erofeev Avrami-Erofeev Prout-Tompkins</li> </ol>	n and A2 A3 A4 B1	growth control) $\begin{bmatrix} -\ln(1-\alpha) \end{bmatrix}^{-1/2} = kt$ $\begin{bmatrix} -\ln(1-\alpha) \end{bmatrix}^{-1/3} = kt$ $\begin{bmatrix} -\ln(1-\alpha) \end{bmatrix}^{-1/4} = kt$ $\ln \frac{\alpha}{1-\alpha} = kt$	$\begin{aligned} x &= 1 - 2 \exp(-kt) \\ x &= 1 - 3 \exp(-kt) \\ x &= 1 - 4 \exp(-kt) \\ x &= \frac{\exp(kt)}{1 + \exp(kt)} \end{aligned}$
<ol> <li>Deceleratory rate equations</li> <li>Based on diffusion mechanism One-dimensional diffusion Two-dimensional diffusion Three-dimensional diffusion Ginstling-Brounshtein Anti-Jander (counter diffusion)</li> </ol>	n D1 D2 D3 D4	$\begin{aligned} \alpha^2 &= kt \\ (1 - \alpha) \ln(1 - \alpha) &= kt \\ [1 - (1 - \alpha)^{1/3}]^2 &= kt \\ [1 - (2\alpha/3)] - (1 - \alpha)^{2/3} &= kt \\ [(1 + \alpha)^{1/3} - 1]^2 &= kt \end{aligned}$	$\alpha = \sqrt{kt}$ $\alpha = 1 - (1 - \sqrt{kt})^{3}$ $\alpha = (1 + \sqrt{kt})^{3} - 1$
3.2. Based on geometric models Contracting area Contracting volume	R2 R3	$[1 - (1 - \alpha)^{1/2}] = kt$ [1 - (1 - \alpha)^{1/3}] = kt	$\alpha = 1 - (1 - kt)^2$ $\alpha = 1 - (1 - kt)^3$
3.3. Based on order of reaction First order Second order Third order	F1 F2 F3	$-\ln(1 - \alpha) = kt$ $1/[1 - \alpha] = kt$ $1/[1 - \alpha]^2 = kt$	$\alpha = 1 - \exp(-kt)$ $\alpha = 1 - \frac{1}{kt}$ $\alpha = 1 - \frac{1}{\sqrt{kt}}$

 Table 1

 Commonly used solid-state reaction mechanisms

where  $g(\alpha)$  is a function of the fraction reacted at time t at an arbitrary constant temperature.

The function  $g(\alpha)$  can take different forms depending on the type of reaction that occurs, and such forms have been reviewed by Brown and co-workers [2,3]. A summary of these functional forms is given in Table 1. One way of obtaining k is to calculate all the available functions of  $g(\alpha)$  and to find the one which gives the best linear compliance with Eq. (1). Most of the methods so far reported in the literature make use of  $\alpha$ , which is the fraction converted and is measured by means of any property p that changes linearly and continuously with the reaction during the course of an isothermal experiment as a function of time. The property chosen must be sufficiently sensitive to represent the change of the state and must be linearly proportional to the number of reactant or product molecules. In thermal analysis, such a property which is monitored as a function of time can be any one of the following, viz.: the instantaneous weight during thermogravimetry, the intensity of a characteristic line in high temperature X-ray diffractometry, the enthalpy in dynamic calorimetry, the volume in thermomechanical measurement, or the physical dimension in dilatometry. The term  $\alpha$  is generally defined by

$$\alpha = \frac{|(p_t - p_0)|}{|(p_{\infty} - p_0)|} = \frac{\Delta p_t}{\Delta p_{\infty}}$$
(2)

where  $p_t$  is the value of the property at any instant of time,  $p_0$  is the value of the property at the initial time, and  $p_{\infty}$  is the value of the property after infinite time (symbolizing completion of the reaction).

In general, the methods of kinetic analysis are based on the very definition of  $\alpha$ . That is, one can compute the fraction converted only with the knowledge of  $p_{\infty}$  after completion of the reaction. Quite often one comes across situations where reactions in a solid medium seldom proceed to completion for a variety of reasons, such as low temperature and limitations in the solid-state transport processes. Such reactions designated as incomplete reactions are therefore unsuitable for the determination of kinetic constants because of their dependence on the numerical value of  $p_{\infty}$ . However, the present trend of computer based automation-cum-data processing could facilitate the determination of kinetic constants, even without recourse to the value of  $p_{\infty}$ , if the mathematical solutions could be suitably reformulated. The steps involved in such an approach are described in this work, along with its application to a numerically simulated TG curve for the purpose of illustration.

#### 2. Mathematical formulation

Eq. (1) above can be rewritten as

$$\alpha = f(k,t) \tag{3}$$

and various  $g(\alpha)$  equational forms listed in Table 1 correspond to different mechanisms. For two distinct instants of time  $t_1$  and  $t_2$ , Eqs. (2) and (3) yield

$$\alpha_{t1} = \Delta p_{t1} / \Delta p_{\infty} = f(k, t_1) \tag{4}$$

$$\alpha_{t2} = \Delta p_{t2} / \Delta p_{\infty} = f(k, t_2) \tag{5}$$

The ratio of the weight changes R is obviously given by the ratio of  $\alpha_{t1}$  and  $\alpha_{t2}$ 

$$R = \Delta p_1 / \Delta p_2 = f(k, t_1) / f(k, t_2)$$
(6)

Eq. (6) can be solved algebraically for k for the different mathematical forms of  $g(\alpha)$  in Table 1, and such solutions are summarized in Table 2. It should be noted at this juncture that, for all except a few of the mechanisms, the algebraic solutions could be found in the present study.

The exceptional cases are mainly those mechanisms based on nucleation and growth, such as Avrami-Erofeev equations, which have exponential terms rendering algebraic solutions difficult, if not impossible. However, the numerical solution, viz., the Newton-Raphson approach, can be employed for elucidating the roots of Eq. (6) when an analytical route is not feasible. A brief description of this iteration method, along with initial guessed values, are given in the Appendix. In addition, the rate equations based on a power law, such as  $\alpha^{1/n} = kt$ , cannot be solved for an exclusive k. Instead, the algebraic roots lead to n, the power law exponent, and  $k^n$ 

Analytical solutions for k with weight	t ratio R		
Rate mechanisms		Solution for rate constant $k$	Remarks
1. Accelerating rate equations		<u>.</u>	
Power law	PI	$n = \ln(R)/\ln(t_1/t_2)  k \Delta w_{\infty}^{1/n} = \frac{\Delta w_{T'}}{t_1}$	$k\Delta w_{\infty}^{1/n}$ could not be separated
Exponential law	E1	$k = \frac{\ln(R)}{(t_1 - t_2)}$	
2. Sigmoid rate equations			
Avrami-Erofeev	<b>A</b> 2	$(R-1) + 2 \exp(-kt_1) - 2 \exp(-kt_2) = 0$	Solution can be obtained by
Avrami-Erofeev	A3	$(R-1) + 3 \exp(-kt_1) - 3 \exp(-kt_2) = 0$	Newton-Raphson method. Refer
Avrami – Erofeev	A4	$(R-1) + 4 \exp(-kt_1) - 4 \exp(-kt_2) = 0$	to appendix for the method
Prout-Tompkins	BI	$0 = \frac{\exp[k(t_1 - t_2)][1 + \exp(kt_2)]}{[1 + \exp(kt_1)]} - R$	
<ol> <li>Deceleratory rate equations</li> <li>Based on diffusion mechanism</li> </ol>			
One-dimensional diffusion Three-dimensional diffusion	D1 D3	Solution is similar to power law with $n = 0.5$ $(Rt_2^{3/2} - t_1^{3/2})k - (Rt_2 - t_1)\sqrt{k} \cdot 3 + 3(Rt_2^{0/5} - t_1^{0/5}) = 0$	
Anti Jander (counter diffusion)		$(Rt_2^{3/2} - t_2^{3/2})k + (Rt_2 - t_1)\sqrt{k \cdot 3} + 3(Rt_2^{0.5} - t_1^{0.5}) = 0$	
3.2. Based on geometric models			
Contracting area	R2	$k = rac{2t_1 - 2Kt_2}{t_2^2 - t_2^2 R}$	
Contracting volume	R3	$(Rt_{2}^{3} - t_{1}^{3})k^{2}^{2} - (Rt_{2}^{2} - t_{1}^{2}) \cdot 3k + 3(Rt_{2} - t_{1}) = 0$	
3.3. Based on reaction order			
First order	FI	$R[1 - \exp(-kt_2)] - [1 - \exp(-kt_1)] = 0$	Newton-Raphson method can
Second order	F2	$k = \frac{(Q-1)}{(Qt_2 - t_1)}$	be used to obtain rate constant
Third order	F3	$k = \frac{(Q^* - 1)^2}{[(Q^*)\sqrt{t_1} - \sqrt{t_2}]^2}$	

. Table 2 Note:  $R = \Delta w_1 / \Delta w_2$ ;  $Q = Rt_1 / t_2$ ;  $Q^* = R \sqrt{t_1 / t_2}$ .

.

Time/s	Delta $W(\Delta W)$ values for						
	Fig. 2	Fig. 1					
10	1.3216	0.2151					
70	3.2341	1.4117					
130	4.2075	2.4619					
190	4.9025	3.3838					
250	5.4482	4.1929					
310	5.8977	4.9030					
370	6.2789	5.5263					
430	6.6086	6.0734					
490	6.8980	6.5536					
550	7.1546	6.9751					
610	7.3942	7.3450					

Table 3 Numerical values of hypothetical TG curves chosen for Figs. 1 and 2

Note:  $\Delta W_{\infty} = 10.0000$ .

multiplied by  $\Delta p_{\infty}$ , as is pointed out in Table 2. Further, some of the equations which are based on diffusion controlled mechanism (viz., the Ginstling-Brounshtein equation D4 and two-dimensional diffusion D2, have defied all our attempts at solution for their roots. Perhaps the following polynomial approximation suggested by Bar-Gadda [4] may lead to solutions of the D4 and D2 equations.

### 2.1. Evaluation of k with numerical simulation

Two hypothetical TG curves as given in Table 3 are taken for testing the analytical solutions listed in Table 2. Both the approaches developed in the earlier section, viz., those of analytical solutions and numerical methods, have been applied to the different models and the values of k have been computed as a function of time. Typical results of such computations are presented in Fig. 1(a)-(d). In the case of the mechanism that is operative for the reaction under investigation, k has to be independent of time. If k does not have a constant value, this indicates that the mechanism under consideration is not operative. In addition to these two distinct categories, possibilities exists for marginal variation of k with time, which makes it difficult to select between the two options (see Fig. 2(a)-(d)). Under these circumstances, one resorts to the computation of  $\alpha$  and  $\Delta p_{\infty}$  using the derived values of k. A cursory look at the values of  $\alpha$  and  $\Delta p$  calculated thus will usually reveal the acceptability or otherwise of the mechanism being considered. This point is illustrated with the help of Table 4. It is obvious that values of  $\alpha$  that are either greater than unity or negative and those values of  $\Delta p_{\infty}$  noncomparable in magnitude to the values of  $\Delta p_0$  or nonconstancy of  $\Delta p_{\infty}$  are untenable. It is thus easy to reject the mechanisms that have given rise to such k values.

In this manner, numerical simulation has been carried out on all fourteen mechanisms, and it is found that the present on-line method can be readily adopted



mechanism is only approximate value.

Fig. 1. (a), (b).



Fig. 1. Illustration of the method for generation of the rate constant k vs. time t using the data of the hypothetical TG curve (Table 3), which is following the F1 reaction mechanism for various reaction mechanisms: (a), based on reaction order; (b), based on nucleation and growth; (c), based on diffusion and geometric models; (d), based on accelerating rate expressions.



mechanism is only approximate value

Fig. 2. (a), (b).



Fig. 2. Plot of computed rate constant k as a function of reaction time t for the hypothetical TG curve which is following the D3 reaction mechanism, which exhibits marginal variation of k with time for certain reaction mechanisms among various reaction mechanisms: (a), based on reaction order; (b), based on nucleation and growth; (c), based on diffusion and geometric models; (d) based on accelerating rate expressions.

Table 4 Computed  $\alpha$  values and final weight loss  $\Delta W$  for D3, F3, R3, A4 and anti-Jander mechanisms (which exhibited marginal variation in k vs. t plots; Fig.

2) using th	is computed k	c for the respe	ctive mechanism	a by this on-li	ne method fron	n the hypothetic	cal TG curve, wh	nich follows the l	D3 mechanism	
3-D diffus mechanisn	ion 1 D3	Third orde mechanism	er reaction 1 F3	Contractin mechanism	g volume 1 R3	Avrami-Ero mechanism A	feev A4	Anti-Jander Counter diffu	3-dimensional sion mechanism	
8	$\Delta W_{\infty}$	×	$\Delta W_{\infty}$	ж	$\Delta W_x$	к	$\Delta W_{x}$	8	$\Delta W_{\infty}$	
0.3234	10.001	0.7357	4.3962	1.0021	3.2274	-2.3003	-1.4060	-0.3234	- 10.001	
0.4207	10.0000	0.6106	6.8906	0.9658	4.3564	-2.4792	- 1.6971	-0.4207	-10.000	
0.4902	10.0000	0.5958	8.2287	0.9479	5.1718	-2.5313	-1.9368	-0.4902	-10.000	
0.5448	10.0000	0.5949	9.1585	0.9421	5.7827	-2.5637	-2.1251	-0.5448	-10.000	
0.5898	10.0000	0.5984	9.8561	0.9410	6.2676	-2.5884	-2.2785	-0.5898	-10.000	
0.6279	10.0000	0.6037	10.4003	0.9418	6.6666	-2.6089	-2.4067	-0.6279	-10.000	
0.6609	10.0000	0.6100	10.8343	0.9437	7.0032	-2.6269	-2.5158	-0.6609	-10.000	
0.6898	10.0000	0.6167	11.1852	0.9459	7.2922	-2.6430	-2.6099	-0.6898	-10.000	
0.7155	10.0000	0.6237	11.4710	0.9484	7.5436	-2.6577	-2.6920	-0.7155	-10.000	
0.7384	10.0000	0.6309	11.7046	0.9510	7.7646	-2.6714	-2.7642	-0.7384	-10.000	

to clarify the mechanism that is operative in the condensed phase reaction without waiting for the completion of the reaction.

# 3. Application of on-line method to real TG curves

The foregoing discussion on numerical simulation has been restricted to a hypothetical TG curve instead of a real one. Nevertheless, the on-line method can be readily adapted to real experimental TG curves if the following precautions are taken.

(a) The weight record should be devoid of apparent weight changes, as achieved by suitable incorporation of blank corrections during the TG run itself, in order to derive the full benefit of the on-line method. It must be mentioned that the zero-time corrections should be also carried out a priori so that the initial weight change  $\Delta p_0$ is free from error. A mathematical method for correcting zero-time errors during the course of the isothermal experiment itself is under development [5].

(b) The weight record should be a sufficiently smooth one, free from fluctuations, as could be attained by incorporation of computer programs based on Fourier analysis; otherwise, erratic values of k might be obtained.

Even though the above method is applicable for any isothermal experiment, in general thermogravimetry constitutes a major field of activity for high temperature solid-state kinetic studies, which in turn encompass many high temperature factors (e.g., compatibility, decomposition, corrosion, preparation, degradation etc.). Application of the above method to experimental techniques other than thermogravimetry should be possible provided that the change in the relevant property is smooth and devoid of "apparent" changes, and also free from zero-time errors or with the possibility of in situ correction of such errors.

#### Acknowledgment

The authors are profoundly thankful to Shri. J.B. Gnanamoorthy, Head, Metallurgy Division, for his kind encouragement to carry out this work.

#### Appendix: Newton-Raphson method of finding the root

Consider  $x = x_1$  as a known rough approximation to a root of f(x) = 0. Suppose that the exact root is at  $x = x_1 + h$ , so that  $f(x_1 + h) = 0$ . As h is a small value compared with x, by Taylor's expansion

$$f(x_1 + h) = 0 = f(x_1) + hf'(x_1) + h^2/2!f''(x_1) + \dots$$

Neglecting terms in  $h^2$  and other higher order terms results in

$$h \approx -f(x_1)/f'(x_1)$$

Table A1

Initial approximate	e roots for	various	mechanisms	which	depend	on	the	Newton-	Raphson	method	for
the solution of the	rate const	tant k									

Mechanism	Initial root k for iteration purpose				
A2	$k = \frac{(1-R)}{2(t_1 - Rt_2)}$				
A3	$k = \frac{(1-R)2}{3(t_1 - Rt_2)}$				
A4	$k = \frac{(1-R)3}{4(t_1 - Rt_2)}$				
R3	$k = \frac{(Rt_2 - t_1)}{(Rt_2^2 - t_1^2)}$				
B1	$t_2(t_1 - t_2)k^2 + (2t_1 - Rt_1 - t_2)k + 2(1 - R) = 0$				

Note: the above equations are not analytical solutions for the rate-constant, since they are obtained by ignoring some terms (higher order terms in expansion).

where  $f'(x_1)$  is the value of the differential coefficient of f(x) at  $x = x_1$ . Consequently, a second approximation to the root is

$$x_2 = x_1 + h = x_1 - \frac{f(x)}{f'(x_1)}$$

This approach may be used iteratively for improving the approximate root to the desired degree of accuracy. The initial approximate roots for iteration purpose for the rate mechanisms that are controlled by nucleation and growth are given in Table A1.

#### References

- [1] H.P. Nawada, Thermochim. Acta, 242 (1994) 239.
- [2] M.E. Brown, Introduction to Thermal Analysis, Techniques and Applications, Chapman & Hall, London, 1988, p. 127.
- [3] M.E. Brown D. Dollimore and A.K. Galwey, Reactions in the solid state, in C.H. Bamford and C.F.H. Tipper (Eds.), Comprehensive Chemical Kinetics, Vol. 22, Elsevier, Amsterdam, 1980, pp. 41-113.
- [4] R. Bar-Gadda, Thermochim. Acta, 34 (1979) 161.
- [5] H.P. Nawada and O.M. Sreedharan, to be published.